## Saw-toothed Distributions of Deuterium in Butenes Formed by 1,3-Butadiene Deuteration on a Pt/Al<sub>2</sub>O<sub>3</sub> Catalyst in D<sub>2</sub>SO<sub>4</sub>

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Saw-toothed distributions of deuterium are observed in butenes produced by the deuteration of 1,3-butadiene on  $Pt/Al_2O_3$  catalysts suspended in 0.5 M  $D_2SO_4$ . The nature of the saw-tooth is sensitive to the purity of the solution and to the deuterium content of the solution. On the basis of the N-profiles (the distributions of hydrogen equilibrated with surface H/D pool) deduced from the observed distributions of deuterium in butenes, the saw-tooth distribution is explained by the reaction mechanism where cis- and trans-1-methyl- $\pi$ -allyls are reaction intermediates for the formation of cis-2-butene and the other isomers of 1-and trans-2-butenes respectively.

The heterogeneous catalytic hydrogenation of 1,3butadiene in the gas phase has widely been studied on various transition-metal catalysts from the 1960's, for example, on Pt,1-4) Pd,1-3,5) other noble metals,1-4) Co<sup>6-8)</sup>, and Ni.<sup>6,8,9)</sup> However, only a few of these studies have used an isotopic tracer method. The deuteration of 1,3-butadiene on Pt catalysts has been reported only by Bates et al.3) Their reaction mechanism includes mono- and di- $\pi$ -bonded butadiene as the raction intermediates. 1,3-Butadiene is first chemisorbed in the mono- $\pi$ -bonded form and then some of the adsorbed 1,3-butadiene becomes the di- $\pi$ -bonded one in an irreversible way. Thereafter, these adsorbed butadienes, in equilibrium with the corresponding adsorbed butenyl intermediates, are converted to butenes. Their discussion was based on the Nprofiles calculated from the distribution of the deuterium in the products.

One must mention that in gaseous catalytic deuteration, deuterium up-take is limited to a lower extent because of the lower deuterium-fraction in adsorbed hydrogen atoms, fD, due to both the slow rate of the exchange reaction of the adsorbed hydrogen with D23,10) and the smaller ratio, D in D2 gas/H in butadiene. This limitation is entirely removed in the case of the reaction in a deuterated acid solution.<sup>11)</sup> That is, f<sub>D</sub> is raised nearly to unity through the fast equilibrium step;  $D(a) = D^{+} + e^{-}$  on Pt, and the ratio of D in solution/H in butadiene is extremely large. Thus, the reaction products in a solution of deuterated acid are expected to acquire many more deuterium atoms and to provide more concrete information for the elucidation of the reaction mechanism. We have already reported the deuteration of 1,3-butadiene on Pt/graphite<sup>11)</sup> and Pt-net,<sup>12)</sup> of ethylene<sup>13)</sup> and propene<sup>14)</sup> on Pt in a 0.5 M D<sub>2</sub>SO<sub>4</sub> solution. The deuteration of cyclopentene in solutions of tetrahydrofuran (THF) containing D<sub>2</sub>O with and without 5% D<sub>2</sub>SO<sub>4</sub> or in the other solutions of CH<sub>3</sub>COOD, CH<sub>3</sub>OD, (CH<sub>3</sub>)<sub>3</sub> COD, and DOCH<sub>2</sub>CH<sub>2</sub>ND<sub>2</sub>-CH<sub>3</sub>OD has been studied by Phillipson and Burwell, 15) but here the f<sub>D</sub>'s are lower than that in a deuterated acid solution, and hence the average number of deuterium atoms taken up in the product cyclopentane was much smaller, even though the addition of D<sub>2</sub>O to THF accelerated the deuterium-exchange reaction.

In the present investigation, the deuteration of 1,3-butadiene on a Pt/Al<sub>2</sub>O<sub>3</sub> catalyst was conducted in 0.5 M D<sub>2</sub>SO<sub>4</sub> purified by the preelectrolysis. We will present a new saw-toothed distribution of deuterium in butenes and discuss the reaction mechanism.

## **Experimental**

Catalysts. The Pt/Al<sub>2</sub>O<sub>3</sub> (0.5 wt% Pt) used in this study was a reference catalyst supplied by the Catalysis Society of Japan and was prepared as follows. <sup>16)</sup> The  $\gamma$ -alumina (BET surface area, 174 m<sup>2</sup>/g; pore volume, 0.66 ml/g) was impregnated in an aqueous solution of H<sub>2</sub>PtCl<sub>6</sub> and then dried overnight. After calcination at 450 °C for 3 h in O<sub>2</sub>, the catalyst was reduced in a H<sub>2</sub> stream at 300 °C for 3 h and then recalcinated at 600 °C for 3 h. The dispersion of Pt has been measured by means of the CO, H<sub>2</sub>, and O<sub>2</sub> adsorption methods by several investigators and found to be ca. 0.6, though slightly scattered. <sup>16)</sup>

Reaction Procedure. The catalyst  $(0.1-0.2\,\mathrm{g})$ , heated at 250 °C for 1 h in a H<sub>2</sub> stream, was suspended in 0.5 M D<sub>2</sub>SO<sub>4</sub> and rereduced by bubbling D<sub>2</sub> (Showa Denko, 7N-purity, 99.97D%,  $P_{\mathrm{D}}=13\,\mathrm{mmHg}$ , 1 mmHg=133.3 N·m<sup>-2</sup>) through the solution. The reaction gas was mixture of 1,3-butadiene (4N-purity,  $P_{\mathrm{R}}=14\,\mathrm{mmHg}$ ), D<sub>2</sub>( $P_{\mathrm{D}}=7$  or 28 mmHg) and He (7N-purity) at a total pressure of 1 atm. The reaction was conducted by circulating the reaction gas through the solution at 20±1 °C. Our previous work has shown that, under these conditions, the diffusion of D<sub>2</sub> to the catalyst surface is rate-determining. No reaction occurred under these conditions without the catalyst.

Solution. The solution of 0.5 M D<sub>2</sub>SO<sub>4</sub> was prepared from D<sub>2</sub>O (Showa Denko, 99.75D%) and sulfuric acidd<sub>2</sub> (Merck 99D%). The deuterium content of the solution was estimated from its specific gravity. Unless otherwise stated, the solution was subjected to preelectrolysis overnight (anodically and then cathodically, several mA). The AES and XPS of the Pt electrode used for the preelectrolysis were run on an ESCA 3 Electron Spectrometer (VG Scientific, Ltd.) to detect any impurity picked up from the solution. Both the purity and the deuterium content of the solution greatly influenced the results. These effects will be discussed in the text.

Analysis. The analyses of the products were conducted gas-chromatographically and mass-spectrometerically, as has been described previously.<sup>11)</sup>

<sup>&</sup>lt;sup>1</sup> 1 M=1 mol dm<sup>-3</sup>.

## Results and Discussion

Saw-toothed Distribution. Table 1 presents the saw-toothed distributions of deuterium in butenes produced from 1,3-butadiene on 0.5 wt%Pt/Al<sub>2</sub>O<sub>3</sub> in pre-electrolyzed 0.5 M D<sub>2</sub>SO<sub>4</sub> with a high deuterium content (99.7D%). The saw-toothed shape is most clear in trans-2-butene and least clear in cis-2-butene, while the latter product shows the most enhanced deuterium-exchange among the three isomers. Such saw-toothed distributions are independent of the conversion, at least up to 20%. As has been stated above, each butene takes up much more deuterium atoms than it does in gaseous deuteration on Pt catalysts. For example, the average deuterium number, DN,

 $\left(\sum_{i=1}^{8} i \cdot X_{i}, X_{i} \text{ is the fraction of the } d_{1}\text{-species}\right)$  of cis-2-

butene in Table 1 is 5.2, while, it is 2.1 in the gaseous deuteration.<sup>3)</sup> However, the product distributions are very close to each other; butane:1-butene: trans-2-butene:cis-2-butene=44:34:11:12 in this work and 44: 36:10:10 at 15 °C in a gaseous reaction.<sup>1)</sup> This fact indicates that the reaction mechanism is almost the same for both systems. The present saw-toothed distributions have also been observed in our separate experiments on such other catalysts as 5 wt% Pt/Al<sub>2</sub>O<sub>3</sub>, 0.5 wt% Pt/SiO<sub>2</sub>, Pt/TiO<sub>2</sub>, and Pt/Nb<sub>2</sub>O<sub>5</sub> in a deuterated solution.<sup>17)</sup> Therefore, it is concluded that the kind of supports and the amount of doped Pt have no effect on the reaction mechanism.

The saw-toothed shape is sensitive to the solution purity and the deuterium content of the solution. When the solution is used repeatedly without the pre-electrolysis (this was the case in our previous work on Pt/graphite<sup>11)</sup>), the saw-tooth becomes less clear. Such a situation is reproduced in the present catalyst as exemplified by the distribution of deuterium in *trans*-2-butene in Fig. 1 (- $\bigcirc$ -). The overnight pre-electrolysis of the same solution makes the saw-toothed shape clearer, as is shown in Fig. 1 (- $\triangle$ -), indicating that a trace of impurity interferes with the appearance of the saw-toothed shape. In order to check on the impurities removed, the surface of the

Pt electrode used for the preelectrolysis was examined by means of the AES and XPS. Both spectra show the peaks of carbon, oxygen, and sulfur. Since the peak intensity of carbon and oxygen is much the same as that on clean Pt foil, neither kind of atom comes from the solution. The presence of sulfur is easily understood, as it comes from SO<sub>4</sub><sup>2-</sup> in the solution, not from the impurity. The complete absence of the other kinds of atoms in the spectra leads us to assume organic compounds as the impurities in the solution, since organic compounds will be decomposed during the anodic polarization, while inorganic compounds will be deposited through discharge during the cathodic polarization. However, a possibility would remain that the impurity is so small an amount of the inorganic compound that it cannot be detected by means of the AES and XPS. Further

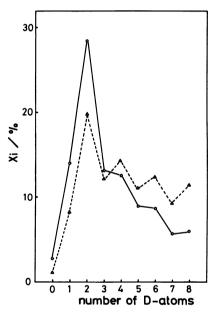


Fig. 1. Distribution of deuterium in trans-2-butene formed by the deuteration of 1,3-butadiene on  $Pt/Al_2O_3$  in 0.5M  $D_2SO_4$  of 98.5D%. The solution; without ( $\bigcirc$ ) and with ( $\triangle$ ) preelectrolysis.  $P_R = 14$  mmHg,  $P_D = 28$  mmHg. Total conversions are 5.1% for  $\bigcirc$  and 7.8% for  $\triangle$ .

Table 1. Distribution of deuterium in butenes obtained by the hydrogenation of 1,3-butadiene on  $Pt/Al_2O_3$  in 0.5 M  $D_2SO_4$  of 99.7 D%, calculated distributions and N-profiles  $P_R=14 \text{ mmHg}, P_D=7 \text{ mmHg}, \text{ total conversion}; 2.0\%$ 

Product	i =	0	1	2	3	4	5	6	7	8	DN	$\mathbf{f_D}$
1-butene	found (X <sub>i</sub> )	0.8	5.9	22.5	15.6	15.9	12.4	9.6	7.8	9.4	4.1	
	calcd (X <sub>i</sub> )	0.2	4.6	22.7	15.6	16.7	12.6	9.5	8.0	9.0		
	N-profile (N <sub>i</sub> )	0.0	0.0	23.0	13.0	17.0	13.0	12.0	0.0	21.0		0.90
trans-2-butene	found $(X_i)$	1.2	6.4	21.0	11.9	14.4	10.9	12.8	8.5	12.9	4.4	
	calcd $(X_i)$	0.2	4.0	22.0	12.5	14.9	11.0	12.6	10.0	12.7		
	N-profile (N <sub>i</sub> )	0.0	0.0	23.0	10.0	16.0	8.0	16.0	0.0	27.0		0.91
cis-2-butene	found $(X_i)$	1.6	3.7	12.9	9.3	10.7	11.2	13.1	14.2	23.4	5.2	
	calcd $(X_i)$	0.0	1.8	13.0	8.9	10.0	11.2	13.4	14.2	23.5		
	N-profile (N <sub>i</sub> )	0.0	0.0	13.0	8.0	9.0	9.0	15.0	0.0	42.0		0.93

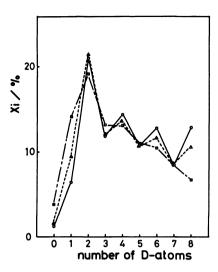


Fig. 2. Distribution of deuterium in trans-2-butene formed by the deuteration of 1,3-butadiene on Pt/Al<sub>2</sub>O<sub>3</sub> in 0.5M D<sub>2</sub>SO<sub>4</sub> of 99.7 D% ( $\bigcirc$ ), 97.6 D% ( $\triangle$ ), and 94.2 D% ( $\square$ ). All the solutions were subjected to the preelectrolysis overnight.  $P_R=14$  mmHg,  $P_D=7$  mmHg. Total conversions are 2.0% for  $\bigcirc$  and 2.5% for  $\triangle$  and  $\square$ .

examination is required for the solution of this problem.

The saw-tooth also tends to be smoothed by decreasing the deuterium content of the solution (Fig. 2). In the solution of 94.2 D%, only the shoulders can be seen at butene- $d_4$  and  $-d_6$ . Though both factors - the solution purity and deuterium content of the solution-influence the saw-toothed shape very much, the lack of the saw-toothed shape in the previous work is taken predominantly as being due to the impurity factor, for the decrease in the deuterium content upon repeated use is not large enough to smoothen out the saw-toothed shape.

Isotopically exchanged 1,3-butadiene was not detected after the reaction. Therefore, it is concluded

that there is an irreversible adsorption of 1,3-butadiene on the Pt surface.

Simulation by N-profile. The N-profiles of butenes were calculated in order to discuss the reaction mechanism. The N-profile consists of  $N_0$ ,  $N_1$ , ...,  $N_8$ , where  $N_i$  represents the fraction of the butene in which i hydrogen positions have been equilibrated with the surface H/D pool. The fraction of molecules in which m out of i equilibrated atoms are deuterium,  $X_m(i)$ , is given by the standard binomial formula as;

$$\mathbf{X}_m(i) = {}_{i}\mathbf{C}_m\mathbf{f}_{D}^{m}(1-\mathbf{f}_{D})^{i-m}$$

Thus, the fraction of  $d_m$ -species,  $X_m$ , is calculated as;

$$\mathbf{X}_m = \sum_{i=m}^{8} \mathbf{X}_m(i) \cdot \mathbf{N}_i$$

The N-profile is determined so that  $X_m$ ,  $m=0, 1, \dots$ , 8, can best fit the observed distribution of deuterium by adjusting  $N_2$ ,  $N_3$ , ...,  $N_8$  ( $N_0=N_1=0$  because the two hydrogen or deuterium atoms are necessarily taken up in butenes).

The N-profiles thus calculated are shown in Table l, together with the experimental and the calculated  $X_m$  distributions of deuterium. The first thing to notice is that each experimental distribution is satis factorily reproduced by the  $X_m$  calculated based on the N-profile listed in the third row for each The N-profiles of 1-butene and trans-2butene. butene resemble each other. Maxima appear at N2, N<sub>4</sub>, and N<sub>8</sub>. N<sub>6</sub> appears as a clear maximum for trans-2-butene, but only as a shoulder for 1-butene. N<sub>7</sub> is exceptionally small in both cases. Thus, the N-profiles of 1-butene and trans-2-butene also reflect the characteristic features of the maxima (or shoulder) at N2, N4, N6, and N8. On the other hand, the Nprofile of cis-2-butene presents three maxima, at N2, N<sub>6</sub>, and N<sub>8</sub>, without N<sub>4</sub>.

N-profile and Reaction Mechanism. The above features of N-profiles are explained by the following reaction mechanism including the reaction intermediates, 3 and 4 proposed by Bates et al.<sup>3)</sup> for the same reaction, but on Pd/Al<sub>2</sub>O<sub>3</sub> in the gas phase;

A molecule of 1,3-butadiene in the gas phase which exists in the s-trans 1 or s-cis 2 form is adsorbed irreversibly on the surface by delocalizing its  $\pi$ -electrons with the same geometrical configuration. The adsorbed s-trans-butadiene is converted to either 1-butene or trans-2-butene through trans-1-methyl- $\pi$ -allyl 3, whereas the s-cis-butadiene is converted only to cis-2-butene through cis-1-methyl- $\pi$ -allyl 4. Interconversions between the two kinds of adsorbed butadienes and between trans- and cis-1-methyl- $\pi$ -allyls are not allowed because of the double-bond-like

nature of the internal C-C bond. The lack of these interconversions is in accordance with the clear difference in the distribution of deuterium between *trans*-and *cis*-2-butene. This difference can not be accounted for by either  $\sigma$ - or  $\pi$ -bonded butadiene, since these adsorbed butadienes allow a rotation of the other vinyl group around the axis of the internal C-C bond and, hence, mutual interconversion between the *trans* and *cis* forms. The  $\sigma$ -bonded butadiene is not likely to be present, as is seen from the negative shift of the work function caused by the butadiene adsorp-

tion on Pt(100) and Pt(111).18)

It must be expected on the basis of the above mechanism that a good correlation exists between the molar fraction of *cis*-2-butene in the products and that of *s-cis*-1,3-butadiene in the gas phase, because *cis*-2-butene is the only product from *s-cis*-1,3-butadiene (butane comes from the *s-trans via* 1-butene<sup>10</sup>). The former molar fraction is 12%, while the latter has been reported to be 3—7%. The correlation is not bad if one takes into account the small modification in the stability of *s-cis*-1, 3-butadiene at the adsorption.

In the above mechanism, the *s*-trans route produces  $d_4$  species by H/D exchange only through Step (1) and  $d_6$  species through Step (1) and also the following Step (3), first proposed by Bates *et al.*<sup>3</sup>;

$$\begin{array}{cccc} \text{CH}_{2}\text{-CH} & \stackrel{(3)}{\longleftrightarrow} & \text{CH}_{2}\text{-CH} \\ * & \text{CH-CH}_{2} & & & \text{CH-CH}_{2} \end{array}$$

The relative rate of the hydrogenation of species 3 to the reverse of Step (1) for 1-butene formation is somewhat faster than the case of *trans*-2-butene formation. Thus, no distinct maximum is observed at N<sub>6</sub> for 1-butene.

On the other hand, the *s-cis* route gives the N<sub>6</sub>-species of *cis-*2-butene through the single step of the reversible Step (2), because the two terminal methylenes in the adsorbed *s-cis*-butadiene are equivalent. Thus, the maximum at N<sub>4</sub> for *cis-*2-butene is diminished.

In addition to  $N_4$  and  $N_6$ , considerable amounts of  $N_3$  and  $N_5$  are obtained. This can be readily explained by the slowness of the reverse rates of Steps (1) and (2).

The high fraction of  $N_8$  and the zero amounts of  $N_7$  for all the butenes suggest the presence of another sequence which causes an extremely fast H/D exchange over a molecule. The above mechanism can not explain the formation of  $N_8$ -species. One possible explanation could be that the butyl intermediate accelerates the H/D exchange by the following, reversible step;

each 
$$C_4H_8 + H \stackrel{(4)}{\longleftrightarrow} C_4H_9$$

where  $C_4H_9$  includes the two possible butyls bonded at either of the carbon atoms of the double bond. Thus, all the hydrogen atoms in the molecule become H/D exchangeable through Steps (1) to (4). The admission of the adsorbed butyl, however, will undoubtedly cause the hydroisomerization of butenes, which is not the case in the hydrogenation of 1,3-butadiene. Further investigation of the details will be required.

The above mechanism is different from that on  $Pt/Al_2O_3$  in the gas phase proposed by Bates *et al.*<sup>3</sup>, where *mono-* and *di-* $\pi$ -bonded butadienes were proposed. Interconversion between these two  $\pi$ -bonded butadienes was taken not to be readily reversible.

Their discussion was based on the N-profiles, which differed for the respective butenes, though the observed distribution of deuterium in 1-butene was very similar to that of trans-2-butene, but different from that of cis-2-butene, as in our results. Therefore, their N-profiles had to lead to a different mechanism. Since the f<sub>D</sub> in the gas-phase deuteration is rather low, it is essentially difficult to calculate the Nprofile accurately from the distribution of deuterium in less deuterated products, though a somewhat sawtoothed figure can be noticed in their N-profile calculated for trans-2-butene. On the other hand, the present system can provide highly deuterium-exchanged products which ensure an accurate Nprofile, and it enables us to elucidate the reaction mechanism more precisely.

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## References

- 1) G. C. Bond, G. Webb, P. B. Wells, and J. M. Winterbottom, J. Chem. Soc., 1965, 3218.
  - 2) P. B. Wells and A. J. Bates, J. Chem. Soc., 1968, 3064.
- 3) A. J. Bates, Z. K. Leszczyński, J. J. Phillipson, P. B. Wells, and G. R. Wilson, J. Chem. Soc. (A), 1970, 2435.
  - 4) P. B. Wells, J. Catal., 52, 498 (1978).
- 5) E. F. Meyer and R. L. Burwell, Jr., J. Am. Chem. Soc., **85**, 2881 (1963).
- 6) J. J. Phillipson, P. B. Wells, and G. R. Wilson, J. Chem. Soc. (A), 1969, 1351.
- 7) B. J. Joice, J. J. Rooney, P. B. Wells, and G. R. Wilson, Discuss. Faraday Soc., 1966, 223.
- 8) M. George, R. B. Moyes, D. Ramanarao, and P. B. Wells, J. Catal., 52, 486 (1978).
- 9) Y. Okamoto, K. Fukino, T. Imanaka, and S. Teranishi,
- J. Catal., 74, 173 (1982).
  10) G. C. Bond, J. J. Phillipson, P. B. Wells, and J. M.
- Winterbottom, Trans. Faraday Soc., 60, 1847 (1964).

  11) H. Kita, K. Shimazu, Y. Kakuno, and A. Katayama-
- Aramata, J. Catal., 74, 323 (1982).
  12) H. Kita, N. Kubota, and K. Shimazu, Electrochim.
- Acta, 26, 1185 (1981).
  13) K. Fujikawa, H. Kita, K. Miyahara, and S. Sato, J.
- Chem. Soc. Faraday I, 71, 1573 (1975).14) K. Shimazu and H. Kita, J. Catal., 86, 129 (1984).
- 15) J. J. Phillipson and R. L. Burwell, Jr., J. Am. Chem. Soc., 92, 6125 (1970).
- 16) Committee on Reference Catalysts, Catalyst Society of Japan, "Reports of 4th Meeting of Reference Catalysts," 1982.
- 17) H. Kita, R. Yoneda, K. Shimazu, H. Hattori, and K. Tanabe, to be published.
- 18) A. E. Morgan and G. A. Somorjai, *J. Chem. Phys.*, **51**, 3309 (1969); G. A. Somorjai, *Catal Rev.*, **7**, 87 (1972).
- 19) L. B. Smith and J. L. Massingil, J. Am. Chem. Soc., 83, 4301 (1961).